

# Mesoporous Ferrihydrite-Based Iron Oxide Nanoparticles as Highly Promising Materials for Ozone Removal\*\*

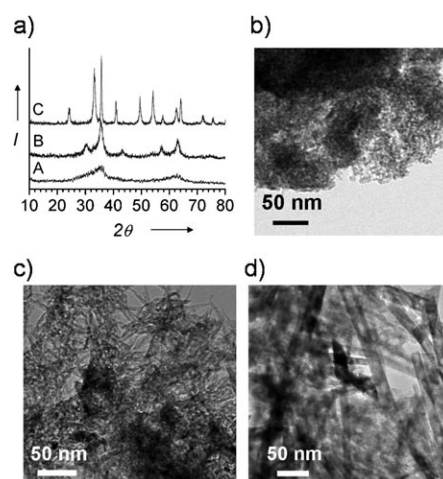
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Gaseous ozone ( $O_3$ ) in the troposphere is considered to be one of the most harmful air pollutants in view of its high reactivity and immediate action to the surroundings, which causes both short- and long-term adverse health effect and also disrupts plant growth.<sup>[1–3]</sup> Materials explored for eliminating  $O_3$  in several applications include activated carbon or carbon-promoted oxide materials, noble-metal-supported catalysts, and various transition-metal oxides.<sup>[3–6]</sup> These materials have diverse drawbacks: they must often be deposited on high-surface-area metal oxides or mixed with organic additives to enhance their performance, they use expensive metal components, they are not very environmentally friendly, and they are not flexible enough to use as a common choice in a wide range of sectors. Herein, we report for the first time that the two-line ferrihydrite (2LFh) with accessible mesopores can be used as a potential candidate for  $O_3$  removal. The following aspects prompted us to consider mesoporous 2LFh (M2LFh) a judicious choice for  $O_3$  removal: 1) it possesses high surface area and, being in the ferrihydrite (Fh) phase, a much higher percentage of iron sites are at or near the surface than in the bulk;<sup>[7–9]</sup> 2) with accessible mesopores, Fh nanoparticles have the potential for high adsorption owing to an increased rate of mass transfer to the reactive iron sites, such as we recently reported for their high efficiency in rapidly removing organic contaminants in the air;<sup>[10]</sup> and 3) as an oxyhydroxide of iron, Fh is environmentally friendly and can be applied in various sectors. We also show herein that the presence of Fh nanoparticles in disordered mesostructured iron oxide has a significant effect on the bulk and surface structure of the material and on the activity. Our findings can contribute toward designing Fh-based materials as new potential catalysts for rapid removal of  $O_3$  and its decomposition.

M2LFh was prepared according to a reported procedure<sup>[10]</sup> by assembly of Fh nanoparticles in 1-propanol in the presence of polyoxyethylene (20) cetyl ether template. Addi-

tionally, a mesostructured semicrystalline iron oxide composed of amorphous Fh nanoparticles and crystalline  $\gamma$ - $Fe_2O_3$  phase (MSIO) and a crystalline iron oxide with no well-defined mesopores (CIO) were prepared for comparison. MSIO was prepared through a sol-gel process in which iron nitrate, oleic acid, a triblock polymer template (F127), and 1-propanol were mixed, with subsequent ageing and calcination. CIO was prepared by assembly of iron oxyhydroxide in a water/ethylene glycol mixture in the presence of cetyltrimethylammonium bromide. Details of MSIO and CIO synthesis are given in the Supporting Information.

The wide-angle XRD pattern of M2LFh (Figure 1a,A) shows two broad reflections of the 2LFh phase. Although the amorphous Fh-phase reflections in the XRD pattern of MSIO



**Figure 1.** a) Wide-angle XRD patterns of A) M2LFh, B) MSIO, and C) CIO. TEM images of b) M2LFh, c) MSIO, and d) CIO.

(Figure 1a,B) were disguised to a great extent by the crystalline peaks of  $\gamma$ - $Fe_2O_3$ , the analysis of the Mössbauer spectrum (see Table S1 in the Supporting Information) indicated that MSIO is composed of about 47% Fh and 53%  $\gamma$ - $Fe_2O_3$ . In the case of CIO, all the diffraction peaks (Figure 1a,C) are in good agreement with the standard XRD pattern of the hexagonal phase of  $\alpha$ - $Fe_2O_3$  (JCPDS No. 80-2377), and the Mössbauer result (see Table S1 in the Supporting Information) gives further confirmation of this characteristic phase. A broad, low-angle XRD peak at  $2\theta = 0.5$ – $3.0^\circ$  (Figure S1 in the Supporting Information) and a characteristic type IV isotherm with a homogeneous pore size distribution in the range 4–6 nm by  $N_2$  adsorption analyses (Figure S2 in the Supporting Information) are critical pieces

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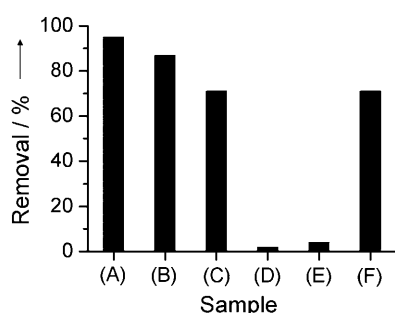
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of evidence that both M2LFh and MSIO are mesoporous. The low-angle XRD reflections observed for M2LFh and MSIO were supported by TEM images. The TEM images illustrate the presence of a disordered mesoporous structure in both cases (Figure 1 b,c). In M2LFh, primary nanoparticles smaller than 10 nm aggregated to form a disordered mesoporous structure. In the case of MSIO, a mixture of spherical and fibrous particles was apparent. Although the above mesoporous characteristics are missing for CIO, the TEM image of CIO illustrates that it crystallized largely as tubular particles with irregular intraparticle pores (Figure 1 d). The Scherrer analysis revealed that the wall structures of MSIO and CIO were made up of particles with an average crystallite size of about 8 and 18 nm, respectively. The BET surface areas of M2LFh, MSIO, and CIO were 180, 140, and 82 m<sup>2</sup> g<sup>-1</sup>, respectively.

Among a wide range of materials tested at room temperature (RT), we found M2LFh to be the most efficient candidate for O<sub>3</sub> removal; it showed about 95 % O<sub>3</sub> removal with high reproducibility (sample A, Figure 2). MSIO (sam-



**Figure 2.** Comparison of the O<sub>3</sub> removal performances of various samples at RT: A) M2LFh, B) MSIO, C) CIO, D)  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>, E) 5 wt % Fe/ZSM-5, and F) commercial MnO<sub>2</sub>.

ple B) effected an O<sub>3</sub> removal of 87 %, whereas CIO (sample C) showed 71 % removal. The O<sub>3</sub> elimination efficiencies of these materials were remarkably better than those of  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> (sample D; 17.5 m<sup>2</sup> g<sup>-1</sup>) and the microporous Fe-incorporated ZSM-5 (sample E, 5 wt % Fe/ZSM-5, 258 m<sup>2</sup> g<sup>-1</sup>); both of these materials showed less than 5 % O<sub>3</sub> removal at RT. Manganese oxide has been reported to be the most active oxide material for O<sub>3</sub> removal and is the commercial catalyst in applications such as electrostatic copying machines.<sup>[3]</sup> In our study, a commercially available manganese oxide based O<sub>3</sub> removal catalyst (sample F, CMD 200, 200 m<sup>2</sup> g<sup>-1</sup>, Chuo Denki Kagaku Kogyo) exhibited only about 71 % removal at RT. The O<sub>3</sub> removal activity of other materials, such as microporous Fe–Si composites, noble-metal-supported catalysts, mesoporous and non-mesoporous oxides, and so forth, are provided in the Supporting Information (see Table S2). All of these materials showed less than 75 % O<sub>3</sub> removal at RT.

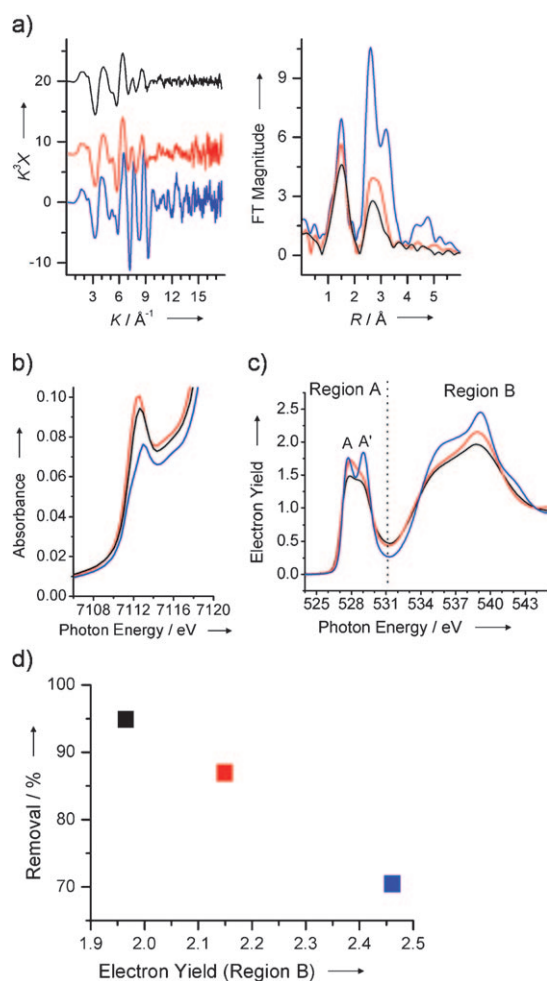
We verified that the non-mesoporous 2LFh (223 m<sup>2</sup> g<sup>-1</sup>) prepared by a conventional route<sup>[8]</sup> was less effective for O<sub>3</sub> removal than M2LFh; it showed only 71 % O<sub>3</sub> removal at RT. This finding demonstrates that the mesoporous structure in M2LFh was advantageous in that it offered an increased

number of exposed surface sites for O<sub>3</sub> adsorption and thereby enhanced performance in O<sub>3</sub> removal. The importance of mesoporous structure and the key role played by Fh nanoparticles in O<sub>3</sub> removal is also evident if the activity of the non-mesoporous  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> (sample D) and MSIO are compared. The latter is mesoporous and contains about 47 % Fh, although it looks like  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> by XRD. MSIO showed about 43.5 times higher O<sub>3</sub> removal rate than  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> at RT. We believe that the mesoporous structure and the characteristics of the Fh phase are useful when other gases or reactants may be included in the air stream, such as when the reaction is carried out in the presence of water vapor or if the air stream contains other contaminants as “spectator” species. For example, among all iron-based materials, M2LFh showed distinctly high activity when O<sub>3</sub> removal was performed at 75 °C with water vapor (see Figure S3 in the Supporting Information).

We have studied the X-ray absorption characteristics of M2LFh, MSIO, and CIO to have knowledge of the relative changes in the surface and bulk structural features of these materials and accordingly of their O<sub>3</sub> removal performance. The Fe K-edge extended X-ray absorption fine structure (EXAFS) analysis showed softened EXAFS oscillations (Figure 3 a, left) and a much lower peak intensity in the corresponding Fourier transformed (FT) spectrum at 2–4 Å (Figure 3 a, right) for both M2LFh (black) and MSIO (red) in comparison with CIO (blue), thus suggesting that a long-range structural order was lacking in mesoporous Fh-based materials.<sup>[10]</sup>

A characteristic pre-edge peak in the Fe K-edge X-ray absorption near-edge structure (XANES) spectra of M2LFh, MSIO, and CIO illustrates the presence of non-centrosymmetric Fe sites in all of them (Figure 3 b).<sup>[11]</sup> Of the three materials in this study, CIO with  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> phase showed the lowest pre-edge peak intensity, because the oxygen atoms in  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> are almost packed with same density around Fe<sup>3+</sup> and thereby offer only a slight distortion in the octahedral (*O<sub>h</sub>*) environment of Fe<sup>3+</sup>.<sup>[12]</sup> Nonetheless, although M2LFh and MSIO have high surface areas and smaller particles with a lot of probable surface imperfection, we found that the pre-edge peak intensities of these materials are lower than that of pure  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>, which contains about 33 % tetrahedral (*T<sub>d</sub>*) iron sites. We believe that the abundant unsaturated Fe sites on the Fh particle surface have different symmetry and coordination number and thereby affect the pre-edge peak feature and its intensity differently. Unlike the case with pure  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>, where the non-centrosymmetric iron sites are more like those in the bulk, the surface-enriched Fe sites in mesostructured Fh-based materials are readily available for adsorption and reaction. Thus, M2LFh showed the highest O<sub>3</sub> removal activity.

Further fruitful information on the electronic states of these materials was obtained by O K-edge near edge X-ray absorption fine structure (NEXAFS) spectroscopy, which is more surface-sensitive than both EXAFS and XANES (Figure 3 c). The NEXAFS spectrum of CIO showed a well-resolved splitting of Fe 3d states into *t<sub>2g</sub>* and *e<sub>g</sub>* symmetry bands in the region A (corresponding to Fe 3d + O 2p bands) with a relatively high peak intensity in the region B (corre-



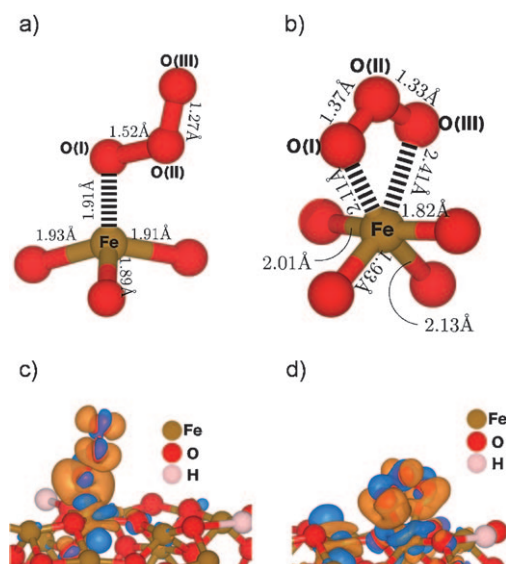
**Figure 3.** a) The Fe K-edge EXAFS spectra (left) and the corresponding FT spectra (right) of M2LFh (black), MSIO (red), and CIO (blue). b) The pre-edge peak from Fe K-edge XANES spectra for M2LFh (black), MSIO (red), and CIO (blue). c) The O K-edge NEXAFS spectra of M2LFh (black), MSIO (red), and CIO (blue). d) A plot of electron yield obtained from the O K-edge NEXAFS peak maximum in the region B (corresponding to Fe 4sp + O 2p states) versus O<sub>3</sub> removal activity for each sample at RT (indicated by the respective color). The activity decreases with relative increase of Fe 4sp contribution to the bonding.

sponding to Fe 4sp + O 2p bands).<sup>[12]</sup> This result is a clear indication of the high packing density of oxygen atoms around iron atoms in CIO. In contrast, the splitting of the 3d state is not well-resolved for M2LFh and MSIO, and a broad peak is detected with decreased intensity of the A' peak feature. This finding is ascribed to the inherent convoluted splitting of iron in different coordination environments with less closely packed oxygen atoms and the presence of more isolated FeO<sub>x</sub> groups<sup>[12]</sup> in M2LFh and MSIO.

Thus, the high O<sub>3</sub> removal activity of mesostructured Fh-based material is due to the abundantly available surface unsaturated iron sites with less oxygen packing around them and the presence of isolated FeO<sub>x</sub> species. Probably the mesoporosity and the presence of the isolated FeO<sub>x</sub> units in M2LFh and MSIO make them more easily reducible than CIO and other crystalline iron oxides (evidenced from

temperature-programmed reduction analysis by H<sub>2</sub>), and accordingly, they showed the highest activity (see Figure S4 in the Supporting Information). This finding is in accordance with the literature, which suggests that an easily reducible metal oxide is more active for O<sub>3</sub> removal and decomposition.<sup>[3]</sup> Furthermore, with respect to CIO, the relatively low peak intensity of the Fe 4sp + O 2p states in Fh-based materials (region B, Figure 3c) and the less dense packing of oxygen around iron sites indicate that the metal electrons in the latter materials are more localized around iron-atom sites. Thus, the Fe 3d + O 2p states with electrons more localized around their iron-atom sites can readily interact with electron-deficient O<sub>3</sub> molecules through both  $\pi$  and  $\sigma$  bonds. Contrarily, with respect to M2LFh and MSIO, the relatively high peak intensity of Fe 4sp + O 2p states of CIO suggests that there is more electron density spread to the weakly structured Fe 4sp states in the latter case. As the electron cloud in Fe 4sp + O 2p states is less localized around iron-atom sites, O<sub>3</sub> interaction with CIO leads to an overall smaller charge transfer from its oxide surface to the O<sub>3</sub> molecule. Thus, a plot of the peak maxima of the Fe 4sp + O 2p states of these iron oxides expressed in electron yield versus O<sub>3</sub> removal activity showed a clear trend that CIO, with the greatest contribution of Fe 4sp states, showed the lowest activity, and vice versa (Figure 3d).

On the basis of the previously proposed calculation model of Fh,<sup>[10]</sup> we have examined the interaction between O<sub>3</sub> and Fh(110) surface by density functional calculations (DFT) to gain a fundamental understanding of the adsorption behavior of O<sub>3</sub> on Fh nanoparticles. The moieties of the most stable structure that resulted after O<sub>3</sub> adsorption on tri- and tetracoordinated Fe sites on the Fh(110) surface are shown in Figure 4a,b. The integrated charge density difference ( $\Delta\rho(r)$ ) for each atom of the O<sub>3</sub>-adsorbed Fh system was calculated (see the Supporting Information for more details). A qualitative picture of the amount of electron transfer during O<sub>3</sub> adsorption on tri- and tetracoordinated iron sites is depicted in Figure 4c,d (the charge flows from blue to orange regions). The extent of charge (electron) transfer from O<sub>3</sub> to Fh (O<sub>3</sub>→Fh) and vice versa (Fh→O<sub>3</sub>) in those adsorbed complexes were examined with Löwdin charge population (LCP) analysis, as reported in the literature.<sup>[13]</sup> This method shows that the charge population of O(I) 2p of O<sub>3</sub> has been increased from 4.26 to 4.59 on O<sub>3</sub> adsorption at tricoordinated iron sites (see Table S3 in the Supporting Information). In contrast, and with respect to gas-phase O<sub>3</sub>, the charge densities of both the terminal oxygen atoms of O<sub>3</sub> at O(I) (O(III)) on tetracoordinated Fe sites has been increased to 4.56 (4.50). We observed that the magnitude of charge transfer from O<sub>3</sub> to Fh was smaller than that of back-donation during the adsorption process in both sites. A comparison of the bond length between gas-phase O<sub>3</sub> (1.28 Å) and adsorbed O<sub>3</sub> revealed that the O(I)–O(II) bond length (1.52 Å) of O<sub>3</sub> on tricoordinated sites has been elongated and that the O(II)–O(III) bond length (1.27 Å) had double-bond character, which is more or less similar to the gas-phase O<sub>3</sub>. This result suggests that O<sub>3</sub> has a strong tendency to dissociate over tricoordinated iron sites, thus producing a reactive atomic “O” and an O<sub>2</sub> molecule (see Figure S5 in the Supporting



**Figure 4.** a) The partial structure derived from the optimized structure of  $\text{O}_3$  adsorbed on Fh(110) tricoordinated Fe site. b) The partial structure derived from the optimized structure of  $\text{O}_3$  adsorbed on Fh(110) tetracoordinated iron site. c, d) Charge density difference  $\Delta\rho(\mathbf{r}) = \rho_{\text{O}_3/\text{Fh}}(\mathbf{r}) - \rho_{\text{O}_3}(\mathbf{r}) - \rho_{\text{Fh}}(\mathbf{r})$  for  $\text{O}_3$  adsorbed on Fh(110), where  $\rho$  is the charge density and  $\mathbf{r}$  denotes the position vector. The charge flows from blue regions to orange regions. c)  $\text{O}_3$  adsorbed on Fh(110) tricoordinated iron site, and d)  $\text{O}_3$  adsorbed on Fh(110) tetracoordinated iron site.

Information for a comparison of density of states of  $\text{O}_3$  before and after adsorption). Although the deformation of  $\text{O}_3$  on tetracoordinated Fe sites was less pronounced than in the case of  $\text{O}_3$  on tricoordinated iron sites, the former case of  $\text{O}_3$  also resulted in elongation of O–O bonds (1.33–1.37 Å) with respect to gas-phase  $\text{O}_3$ . Thus, as previously proposed,<sup>[4]</sup> the  $\text{O}_3$  decomposition on Fh surface may proceed by an Eley–Riedel type mechanism in which the dissociatively adsorbed atomic “O” that was produced on tricoordinated iron sites or the more highly charged  $\text{O}_3$  on tetracoordinated iron sites undergo reaction with another  $\text{O}_3$  molecule from the gas phase, resulting in gaseous  $\text{O}_2$  and reactive peroxide species.

In summary, we have reported for the first time the high efficiency of mesoporous two-line ferrihydrite for  $\text{O}_3$  removal. These studies also demonstrate the promise of the highly favorable electronic and textural structures of mesoporous Fh or Fh-based iron oxides in environmental catalysis, especially

for treating some of the most noxious gases in the atmosphere at moderate reaction conditions. By studying the adsorption and catalytic behavior of such a highly polarizable  $\text{O}_3$  molecule with Fh nanoparticles, it may be possible to gain more insight into the surface structure of Fh, especially as the exact nature of the Fh surface remains ambiguous.

### Experimental Section

$\text{O}_3$  removal measurements were carried out on a fixed-bed down-flow reactor using 0.2 g catalyst material of pellet size 0.5 mm.  $\text{O}_3$  was generated by the electric discharge of  $\text{O}_2$  under a suitable voltage. The resulting ( $\text{O}_2 + \text{O}_3$ ) gas mixture at a flow rate of 0.5 L min<sup>−1</sup> was then mixed with  $\text{N}_2$  gas of flow rate 4.5 L min<sup>−1</sup>, making a total gas flow rate of 5 L min<sup>−1</sup> (initial concentration of  $\text{O}_3$  was 600 ppm). The  $\text{O}_3$  concentration was measured by a chemiluminescence method by treating the residual  $\text{O}_3$  with 1000 ppm NO, and the  $\text{O}_3$  removal was calculated with respect to the initial concentration.

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